## Modeling of Two-phase Flow and Boiling with FLUENT

by

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### Outline

- FLUENT & RELAP5-3D<sup>©</sup> Coupling
- Multiphase models in FLUENT
- Boiling and two-phase flow Case studies with FLUENT
- Summary



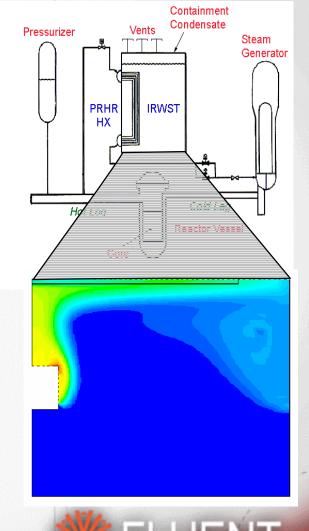
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## **FLUENT & RELAP5-3D<sup>©</sup> Coupling**

#### **Advantages**

- Model entire system using 1 dimensional features of RELAP5-3D<sup>©</sup>
- Model some components of the system in detail using the 3 dimensional features of FLUENT
- Both the system and component behavior is more accurately predicted
- Boundary condition information is transferred back and forth between the two codes



The Right Answer in CFD

## FLUENT & RELAP5-3D<sup>©</sup> Coupling (contd.)

Some key modeling capabilities in FLUENT to be utilized:

- Turbulence
- Two-phase flow
- Flow through packed bed
- Neutronics-fluid interaction in the core region

Focus of this presentation: Two-phase flow



### **Multiphase models in FLUENT**

- Discrete Phase Model (DPM)
- Mixture Model
- Volume of Fluid Model (VOF)
- Eulerian Multiphase Flow Model



#### **Discrete Phase Model (DPM)**

Trajectories of particles/droplets/bubbles are computed in a Lagrangian frame.

-Particles can exchange heat, mass, and momentum with the continuous gas phase.

-Particle-Particle interaction is neglected.

-Turbulent dispersion can be modeled with stochastic tracking or a "particle cloud" model.

- Volume loading: volume fraction < 12%)</li>
- Particulate Loading: Low to moderate.

Application examples: Cyclones, spray dryers, particle separation and classification, aerosol dispersion, liquid fuel and coal combustion. etc.



#### **The Mixture Model**

- Modeling N-phase flows.
- Solves the mixture momentum equation (for mass-averaged mixture velocity)
  - Inter-phase exchange terms depend on relative (slip) velocities
  - Turbulence and Energy equations are solved for the mixture
  - Only one of the phases may be defined as compressible.
- Solves the transport equation of volume fraction for each secondary phase.



#### Applicability of Mixture Model

- Flow regime: Bubbly flow, droplet flow, slurry flow.
- Volume loading: Dilute to moderately dense.
- Particulate Loading: Low to moderate.
- Turbulence modeling: Weak coupling between phases.
- Stokes Number: Stokes Number < < 1.

Application examples: Hydrocyclones, bubble column reactors, solid suspensions, gas sparging.



#### The Volume of Fluid Model (VOF)

- Model to track the position of the interface between two or more immiscible fluids.
- A single momentum equation is solved and the resulting velocity field is shared by all phases.
  - Surface tension and wall adhesion effects can be taken into account.
- Solves transport equation for volume fraction of each secondary phase.
- Recommended that simulation be performed in unsteady mode.



#### **Applicability of VOF Model**

- Flow regime: Slug flow, stratified/free-surface flow.
- Volume loading: Dilute to dense.
- Particulate Loading: Low to high.
- Turbulence modeling: Weak to moderate coupling between phases.
- Stokes Number: All ranges of Stokes number.

Application examples:Large slug flows, filling, off-shore oil tank sloshing, boiling, coating.



#### **The Eulerian Multiphase Model**

- Solves continuity, momentum and energy equations for each phase.
  - Volume fractions characterize equation set for each phase.
    - Several models available to define inter-phase exchange coefficients.
    - Strong coupling makes this model more difficult to use than Mixture Model.
  - Euler Granular option: each granular phase is treated as a distinct interpenetrating granular 'fluid'.
  - Heat and mass transfer between n-phases: Ranz-Marshall (Euler/Euler), Gunn (Euler/granular) and user-defined models.



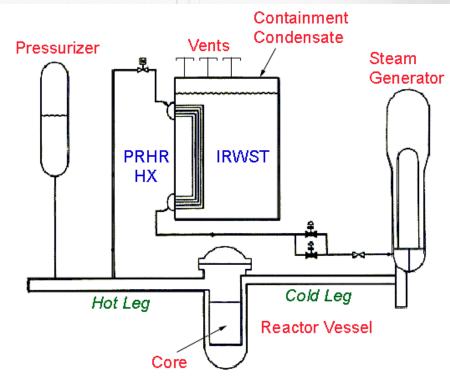
#### **Applicability of Eulerian model**

- Flow regime: Bubbly flow, droplet flow, slurry flow, fluidized beds, particle-laden flow.
- Volume loading: Dilute to dense.
- Particulate Loading: Low to high.
- Turbulence modeling: Weak to strong coupling between phases.
- Stokes Number: All ranges of Stokes number.

Application examples: High particle loading flows, slurry flows, sedimentation, hydro-transport, fluidized beds, risers, packed bed reactors.

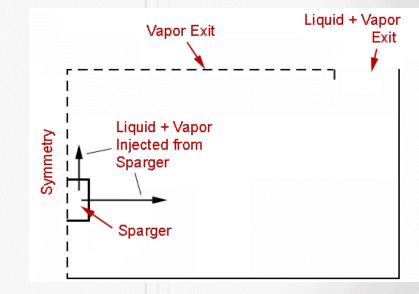
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- The Advanced Pressurized Reactor is light water reactor being designed
- The In-containment Refueling Water Storage Tank (IRWST) is passive safety system for heat removal
- During a small break loss of coolant accident (SBLOCA) it allows steam to cool in a pool of water and escape through vents at the top



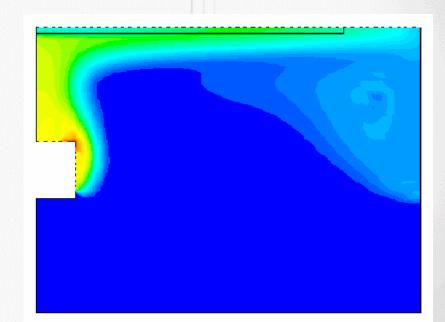


- FLUENT is used to simulate the 2phase flow in the IRWST
- The mixture is injected through a sparger
- The Eulerian multiphase model allows for separate transport equations for
  - liquid (water)
  - vapor (steam)
- The 2D model makes use of a porous region to allow only vapor to exit through most of the top boundary



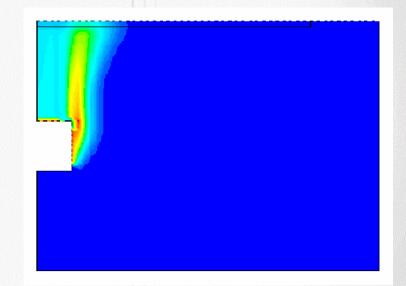


- Steady-state simulations are performed for different bubble sizes and vapor volume fraction
- For 1mm bubbles and 40% vapor at the inlet, most vapor escapes but some is entrained in recirculation in the water near the side of the vessel



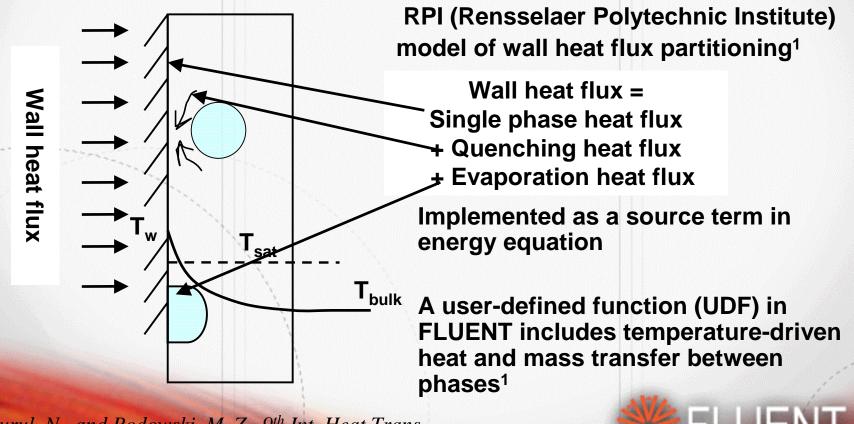


- For 100mm bubbles and 10% vapor at the inlet the flow is very different
- Larger buoyant forces cause steam to rise and escape quickly
- Results suggest that FLUENT is well suited to assist in the design of these systems





#### **Subcooled Nucleate Boiling**



<sup>1</sup>Kurul, N., and Podowski, M. Z., 9<sup>th</sup> Int. Heat Trans. Conf. Jerusalem, p. 21-16, 1990.

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#### **Subcooled Nucleate Boiling**

An annular domain, with heated inner wall is simulated

- FLUENT 6.1 is used to simulate this process for three sets of experimental conditions<sup>2</sup> (below)
- User-defined functions are used with the Eulerian

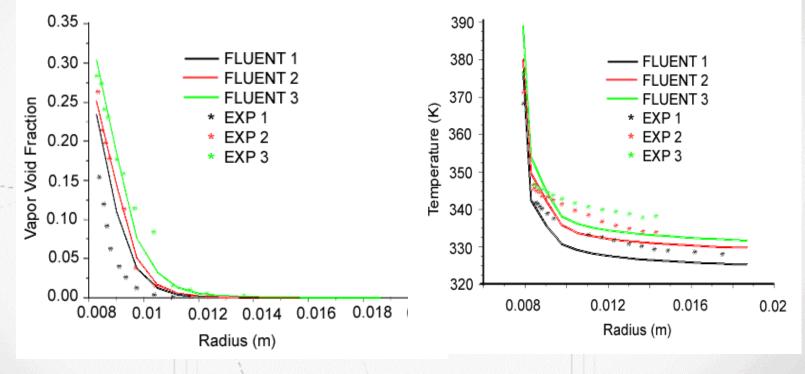
multiphase model to implement the RPI model<sup>1</sup> for

Parameter	EXP 1	EXP 2	EXP 3
Inner wall heat flux, W/m <sup>2</sup>	80,000	95,000	116,000
Fluid mass velocity, kg/m <sup>2</sup> /sec	565	785	785
Mean liquid subcooling at test section inlet, <sup>0</sup> C	37.8	30.3	30.3

<sup>2</sup>Roy, R. P., Velidandla, V., and Kalra, S. P., ASME J. Heat Trans. 119, 754-766 (1997).



#### **Subcooled Nucleate Boiling**



Radial profiles of vapor void fraction prediction

Temperature predictions are in acceptable FLUENT The Right Answer in CFD

### Boiling and two-phase flow Case studies with FLUENT (contd.) Boiling flow in nuclear reactor

Liquid vapor mixture

exits

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 Flow in nuclear fuel assembly

- Pressure 50 atm

- Re<sub>liq</sub>=300,000

Heat flux 0.522 MW/m<sup>2</sup>

Inlet subcooling 4.5 K

- y<sub>+</sub>=100

Liquid enters

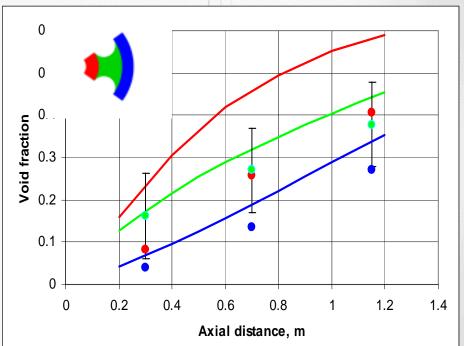
#### **Boiling flow in nuclear reactor**

- Condensation or evaporation at surface of bubbles in free stream
- Turbulent dispersion of bubbles if liquid flow is turbulent
- Additional turbulence created by bubbles
- Modified lift force to account for vortex shedding by bubbles



#### **Boiling flow in nuclear reactor**

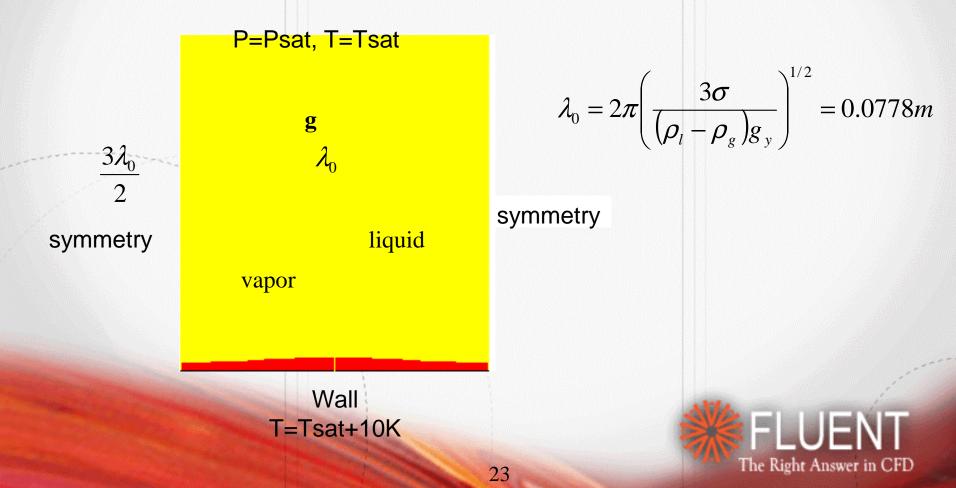
- Wall temperature is defined by bisection method from flux partitioning
- ~3-4 hours to get converged solution on 2GHz CPU 80,000 cells



Comparison with experiment for vapor void fraction



• Using VOF modeling in Fluent



Animation

Contours of volume fraction of the vapor

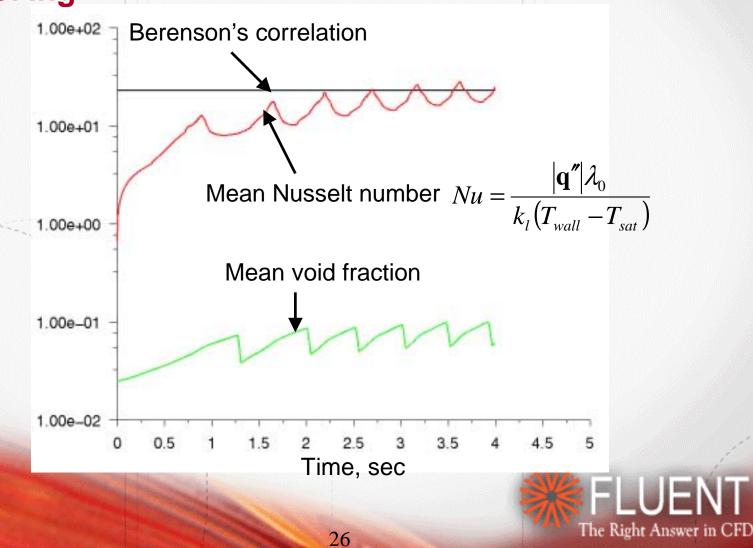


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Velocity

Mass transfer rate, kg/m<sup>3</sup>/sec





## Summary

- Case studies of nucleate boiling and film boiling with FLUENT have been presented.
- These case studies demonstrate that FLUENT can successfully model two-phase flow and boiling.
- Two-phase modeling capabilities will enhance Reactor thermal hydraulic study using FLUENT-RELAP5 coupling

